

In the Claims:

Claim 4 is amended.

1. (canceled)

2. (previously presented) The method according to claim 4, characterized in that at the start-up alkyl benzene and/or the gasoline fraction having a boiling temperature below 220°C is used as an organic solvent.

3. (previously presented) The method according to claim 4, characterized in that a part of the liquid fraction, as subjected to catalytic reforming, with the boiling temperature below 220°C is returned for thermal liquefaction of a new batch of wastes at a pressure in the range from at least 2.9 MPa to not more than 5 MPa, the solvent-waste weight ratio being in the range from more than 1.0 to not more than 3.0.

4. (currently amended) A method for recycling rubber-containing wastes, including thermal liquefaction of wastes fed into a reactor containing an organic solvent at a temperature above 270°C and a pressure up to 6 MPa, separation of the liquid fraction from the undissolved product, distillation of the liquid fraction into the fraction with the boiling temperature below 220°C and the fraction with the boiling temperature above 220°C, characterized in that the process of thermal liquefaction and

thermolysis is carried out in ~~the pseudo-fluidized~~ a fluid bed of the solvent at the organic solvent-waste weight ratio being more than 1.0, the liquid fraction with the boiling temperature below 220°C is subjected to catalytic reforming, a part of the said liquid fraction is used as the target product, and the remaining part of the said fraction is used as a solvent and returned for thermal liquefaction of a new batch of wastes, further all the said process is repeated for many times.